

## SUM-FREQUENCY GENERATION *IN SITU* STUDY OF CO ADSORPTION AND CATALYTIC CO OXIDATION ON RHODIUM AT ELEVATED PRESSURES

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Optical IR-visible sum-frequency generation surface vibrational spectroscopy was employed for *in situ* detection of chemisorbed CO during CO adsorption and catalytic CO oxidation on a rhodium (111) catalyst in the substrate temperature range  $T_s = 300\text{--}800$  K. CO adsorption studies performed over 12 orders of magnitude in CO pressure ( $p_{\text{CO}} = 10^{-8}\text{--}1000$  mbar) demonstrated the reversible molecular adsorption of CO up to a pressure of about 10 mbar. For CO pressures above 10 mbar, the onset of a new irreversible dissociative CO adsorption pathway could be observed already at a substrate temperature of  $T_s = 300$  K. CO dissociation was found to result in the formation of carbon on the surface as the only detectable dissociation product, indicating that CO dissociation occurs via the Boudouard reaction:  $2\text{CO} \rightarrow \text{C(s)} + \text{CO}_2$ . Further experiments were performed to investigate catalytic oxidation of CO under intermediate reagent pressure conditions ( $p_{\text{tot}} = 20$  mbar). The latter experiments were performed under laminar flow conditions in a well-defined stagnation point flow geometry to allow for comparison with numerical reactive flow simulations based on a detailed Langmuir-Hinshelwood (LH) surface reaction mechanism for CO oxidation, including molecular adsorption and desorption of CO and dissociative adsorption of oxygen as well as the formation of  $\text{CO}_2$  through reaction of the adsorbed CO and O species. The good agreement obtained between the results of the CO oxidation experiment and the simulation indicates that for CO and  $\text{O}_2$  partial pressures as typically present in the exhaust gas of spark-ignited internal combustion engines, the Rh(111)-catalyzed CO oxidation can be quantitatively described in the framework of a mean-field approach employing an LH reaction scheme along with kinetics data derived in surface science studies.

### Introduction

Rhodium represents one of the most important catalyst constituents in many industrial processes, such as CO methanation and Fischer-Tropsch synthesis [1,2]. Because of its high efficiency in catalyzing the reduction of NO to  $\text{N}_2$  and the oxidation of CO to  $\text{CO}_2$ , Rh is an essential component of commercial three-way automobile catalytic converters [3]. As a consequence, the adsorption of CO on Rh has been investigated quite extensively under ultra-high vacuum (UHV) conditions [4,5].

However, only a few studies have been reported so far in which CO adsorption on Rh was investigated under actual high-pressure conditions. In recent experiments, optical IR-visible sum-frequency generation (IR-VIS SFG) [6,7] and scanning tunneling microscopy (STM) [8] were employed for *in situ* studies of CO adsorption on an Rh(111) catalyst at room temperature up to a CO pressure of

1000 mbar. The SFG studies demonstrated the appearance of new “low-frequency” CO stretching vibrational features, which could not be observed in previous studies under UHV conditions [6,7]. The new spectral features were assigned to CO molecules terminally adsorbed on defect sites, which were proposed to result from pressure-induced surface roughening of the Rh(111) surface [6]. In Ref. [6], it was further proposed that this process is reversible with respect to CO pressure variation. However, subsequent SFG studies indicated that high CO pressures of about 900 mbar may cause irreversible changes in the Rh(111) surfaces [7]. To shed more light on the actual CO adsorption mechanism, in the present work experiments were carried out in which IR-VIS SFG for *in situ* CO detection in the pressure range  $p_{\text{CO}} = 10^{-8}\text{--}1000$  mbar was combined with “postreactive” Auger electron spectroscopy (AES) studies of the Rh(111) surface. With such an experimental approach, the occurrence of a

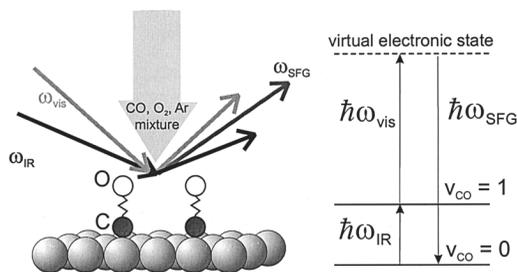


FIG. 1. (a) Schematic illustration of second-order nonlinear optical IR-VIS SFG which was applied in the present study for the *in situ* detection of CO adsorbed on an Rh(111) single-crystal catalyst. (b) Energy-level diagram of the vibrationally resonant IR-VIS SFG process, which allows for surface vibrational spectroscopy of adsorbed CO species.

new high-pressure and high-temperature dissociative CO adsorption pathway has been recently revealed for the CO/Pt(111) system [9,10].

In the present work, this experimental approach was further applied to study heterogeneous CO oxidation on Rh(111) at a CO partial pressure of 2 mbar, as typically present in the exhaust gas of a spark-ignited internal combustion (IC) engine. For comparison with the experimental results, a numerical simulation of the reactive flow system corresponding to the conditions of the experiment was performed, including detailed submodels for molecular transport and surface chemistry.

## Experimental

Experiments were carried out in a reaction chamber, which allows catalytic studies starting from UHV conditions (base pressure  $\sim 3 \times 10^{-10}$  mbar) up to atmospheric pressure. In the elevated pressure regime ( $\geq 1$  mbar), the experimental arrangement can be utilized to investigate reactive processes for well-defined stagnation point flows on catalytic surfaces [11,12]. The chamber was equipped with a quadrupole mass spectrometer (QMS) for thermal-programmed desorption (TPD) measurements, an  $\text{Ar}^+$ -ion sputter source, a four-grid retarding field analyzer for AES and low-energy electron diffraction (LEED) measurements. A second differentially pumped QMS was connected to the exhaust-gas line for on-line monitoring of the stable reaction product  $\text{CO}_2$  [11]. The Rh catalyst (9 mm diameter Rh(111) single-crystal disk, purity 99.99%) could be resistively heated in the substrate temperature range  $T_s = 300\text{--}1600$  K. A clean Rh surface was obtained by applying several cycles of  $\text{Ar}^+$ -ion sputtering followed by oxidation at 1000 K. After the cleaning procedure, residual oxygen was removed and surface

order was restored by annealing the crystal at 1400 K.

For the SFG measurements, a 40 ps mode-locked Nd:YAG laser system was used. A part of its output was frequency doubled to 532 nm and used as the visible input for the SFG process. The other part was used to pump an optical parametric system to generate IR radiation tunable in the frequency range  $\omega_{\text{IR}} = 1800\text{--}2200$   $\text{cm}^{-1}$  with a pulse duration of 25 ps. The IR laser frequency was calibrated to an absolute accuracy of  $\pm 1$   $\text{cm}^{-1}$  by measurements of the gas-phase CO absorption bands around 2143  $\text{cm}^{-1}$  in a reference cell. The visible and IR laser beams were overlapped at the surface, and the SFG signal reflected from the Rh surface was detected by a photomultiplier (Fig. 1). SFG is a second-order nonlinear optical process where a tunable IR ( $\omega_{\text{IR}}$ ) laser beam is mixed with a visible ( $\omega_{\text{VIS}}$ ) laser beam to generate a sum-frequency output ( $\omega_{\text{SFG}}$ ) which is highly specific to the interface region [13]. When the IR beam is tuned over a vibrational resonance of a surface species, the effective surface nonlinear susceptibility is resonantly enhanced and a vibrational spectrum of surface species can be measured [14].

## Results and Discussion

### Pressure Dependence of CO Adsorption ( $p_{\text{CO}} = 10^{-8}\text{--}1000$ mbar)

Figure 2 depicts SFG spectra recorded in the CO pressure range  $10^{-8}\text{--}1000$  mbar together with an SFG spectrum obtained after the pressure was reduced to  $10^{-6}$  mbar. Comparison of the latter spectrum with the one obtained at the same CO pressure in the increasing pressure cycle clearly indicates the non-reversibility of the adsorption process. All spectra shown in Fig. 2 are dominated by a single vibrational feature with CO stretching frequencies in the range  $\omega_{\text{CO}} = 2053\text{--}2075$   $\text{cm}^{-1}$ , typical for terminally bound CO on top of one rhodium surface atom [5]. Further detailed inspection of the spectra (see, e.g., in Fig. 2 the spectra recorded at 500 mbar) revealed a vibrational signal at a frequency of  $1899 \pm 4$   $\text{cm}^{-1}$  originating from CO bound to threefold coordinated hollow sites [5]. The observation of both on-top and hollow-site CO is consistent with the high-pressure Rh(111) +  $(2 \times 2)\text{-}3\text{CO}$  ( $\theta_{\text{CO}} = 0.75$  ML) adsorbate structure derived in the recent STM studies [8]. One monolayer (ML) equals the number of rhodium atoms in the Rh(111) surface plane ( $1.60 \times 10^{15}$  atoms/ $\text{cm}^2$ ). However, due to the reduced sensitivity of SFG for the detection of multiple coordinated CO surface species [15], the relative SFG signal intensities do not reflect the actual on-top versus hollow-site CO coverage ratio of 1:2

of the Rh(111) + (2 × 2)-3CO ( $\theta_{\text{CO}} = 0.75$ ) adsorbate structure [5].

The relative on-top CO adsorbate density,  $n_{\text{on-top-CO}}$  derived from the integrated vibrational band intensity is plotted in Fig. 3a against the CO pressure along with frequency values (Fig. 3b) obtained from the line shape analysis of the on-top CO vibrational bands. For comparison, the pressure dependence of the CO equilibrium surface coverage  $\theta_{\text{CO}}$  is also depicted in Fig. 3c. The variation of the on-top CO adsorbate density with CO pressure and CO equilibrium surface coverage  $\theta_{\text{CO}}$  is in agreement with previous LEED [5] and STM studies [8]. The latter measurements revealed a coverage-dependent shift in the CO adsorption site population from one where all CO molecules are adsorbed at on-top sites (for  $\theta_{\text{CO}} = 1/3$  and below) to one in which CO is adsorbed at on-top and threefold hollow sites with a ratio of 1:3 (for  $\theta_{\text{CO}}$  around 0.57) and finally to one where CO occupies on-top and threefold hollow sites with a ratio of 1:2 (at the CO saturation coverage of 0.75).

The results depicted in Fig. 3b show that when the pressure is increased, the on-top CO stretching vibrational frequency is blueshifted from a value of  $2053 \pm 2 \text{ cm}^{-1}$  at  $p_{\text{CO}} = 10^{-8}$  mbar to value of  $2075 \pm 2 \text{ cm}^{-1}$  for  $p_{\text{CO}} = 10^{-2}$  mbar. In Ref. [6], the observed blueshift was attributed to an increase in the CO-CO vibrational coupling with increasing CO surface coverage (see Fig. 3c). If the CO pressure is further increased, the frequency remains almost constant in the pressure range  $p_{\text{CO}} = 10^{-3}$ –100 mbar, indicating that due to the strong repulsive interaction between the adsorbate molecules, the maximum CO coverage cannot be significantly altered after saturation coverage has been reached (see Fig. 3c). For higher pressures ( $p_{\text{CO}} > 100$  mbar), however, the frequency decreases, finally reaching a value of  $\omega_{\text{CO}} = 2065 \pm 3 \text{ cm}^{-1}$  at  $p_{\text{CO}} = 1000$  mbar. The observed decrease of the on-top CO frequency above  $p_{\text{CO}} = 100$  mbar, which is accompanied by an irreversible decrease of the on-top CO adsorbate density (see Fig. 3a), along with the presence of a considerable carbon signal observed in the “postreactive” Auger spectrum indicated the appearance of a new dissociative high-pressure CO adsorption mechanism (see below).

#### Substrate Temperature Dependence of CO Adsorption

To study the temperature dependence of the CO adsorption on Rh(111), SFG spectra were recorded in the substrate temperature range  $T_s = 300$ –800 K for CO pressures in the range  $10^{-8}$ –100 mbar. In the pressure range  $10^{-8}$ – $10^{-4}$  mbar, adsorbed CO could be detected up to  $T_s = 600$  K, without any indication for dissociation. All SFG spectra could

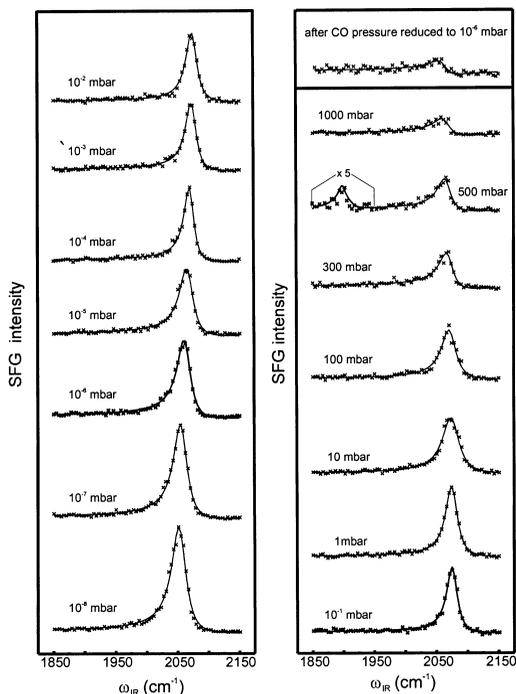


FIG. 2. SFG spectra of CO terminally adsorbed on the Rh(111) single crystal obtained in one single increasing CO pressure cycle in the range  $p_{\text{CO}} = 10^{-8}$ –1000 mbar at a substrate temperature of  $T_s = 300$  K. Spectra were recorded under adsorption/desorption equilibrium conditions by tuning the IR laser over the frequency region  $\omega_{\text{IR}} = 1850$ –2150  $\text{cm}^{-1}$ , in which stretching vibrations of adsorbed CO species can be excited. For comparison, an SFG spectrum recorded after the CO pressure was reduced again to  $p_{\text{CO}} = 10^{-6}$  mbar is shown in the upper right part of the figure. All spectra were normalized to the actual intensity of the IR laser beam at the Rh substrate in order to account for the different absorption of the IR laser radiation by the CO gas phase. The solid lines represent results of numerical simulations of the experimental spectral line shapes which were employed to derive the integrated vibrational band intensity and the stretching vibrational frequency,  $\omega_{\text{CO}}$ , of the on-top adsorbed CO surface species (for details see, e.g., [14]).

be well described by a single vibrational resonance originating from on-top adsorbed CO species (see Fig. 4a). At higher pressures ( $p_{\text{CO}} = 1$  mbar) and substrate temperatures, however, an additional low-frequency vibrational feature which marks the onset of irreversible CO adsorption became observable, as can be seen in Fig. 5a. The dissociative adsorption of CO at higher substrate temperatures is demonstrated by the SFG and Auger electron (AE) data reproduced in Fig. 6.

The SFG spectrum shown in Fig. 6a was recorded

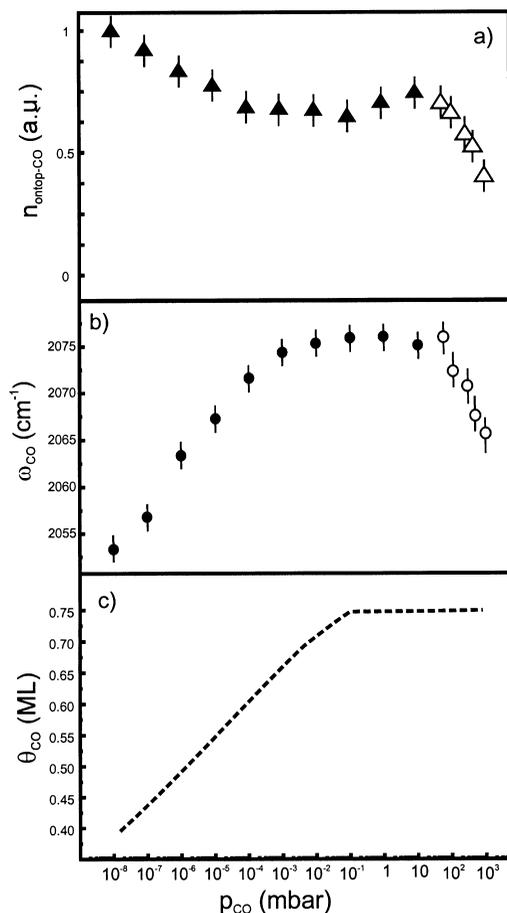


FIG. 3. (a) Relative on-top CO adsorbate density,  $n_{\text{ontop-CO}}$ , derived from the integrated vibrational band intensity of the SFG spectra shown in Fig. 2. In the determination of  $n_{\text{ontop-CO}}$ , it was taken into account that the integrated SFG intensity is proportional to the square of the on-top CO adsorbate density [15]. (b) Stretching vibrational frequency,  $\omega_{\text{CO}}$ , of the on-top adsorbed CO molecules. The open symbols in (a) and (b) indicate the pressure range in which irreversible CO adsorption occurs. (c) CO equilibrium surface coverage,  $\theta_{\text{CO}}$ , calculated using the adsorption/desorption kinetics data for molecular adsorption of CO on Rh(111) given in Table I. Values are plotted against the CO gas-phase pressure.

at a CO pressure of 1 mbar at  $T_s = 300$  K. The spectrum depicted in Fig. 6b was obtained after the substrate temperature was increased to 680 K. In this case, the lower SFG intensity predominately reflects the fact that with increasing substrate temperature the equilibrium CO coverage decreases, which also explains the observed redshift of the center frequency of the on-top CO stretching vibrational band. Nevertheless, a second feature on the

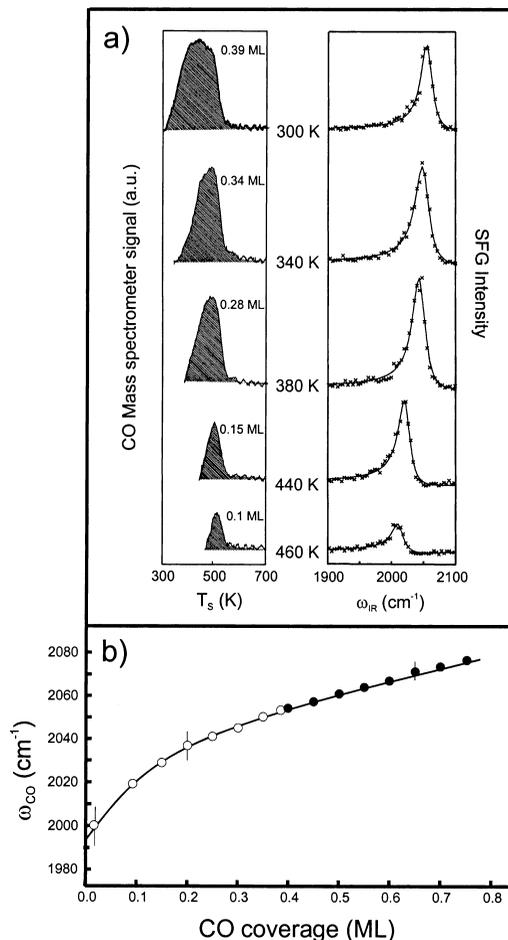


FIG. 4. (a) Right side: Typical SFG spectra of on-top CO surface species on Rh(111) recorded at different substrate temperatures at a fixed CO pressure of  $10^{-8}$  mbar. The SFG intensity is plotted versus the frequency of the tunable IR laser. Experimental data points are represented by crosses, and solid lines represent results of numerical simulations of the experimental spectral line shapes used to determine the coverage dependence of the on-top CO stretching vibrational frequency  $\omega_{\text{CO}}$ . Left side: TPD spectra of CO measured under molecular flow conditions at a CO pressure of  $10^{-8}$  mbar. TPD spectra were recorded right after the corresponding SFG measurements (shown on the right side) were obtained. Desorption was started at different substrate temperatures as indicated in the figure. The surface coverages given in the figure were derived from the integrated areas of the TPD spectra and normalized to the value at the saturation coverage ( $\theta_{\text{CO}} = 0.39$  ML) at 300 K (for details, see [11]). (b) Coverage dependence of the stretching vibrational frequency,  $\omega_{\text{CO}}$ , of the on-top adsorbed CO molecules. Open circles represent values derived from combined SFG and TPD measurements as illustrated in (a). Filled circles represent results of room-temperature adsorption studies carried out in the CO pressure range  $p_{\text{CO}} = 10^{-8}$ –10 mbar for which reversible molecular adsorption of CO occurs (see text and Fig. 2).

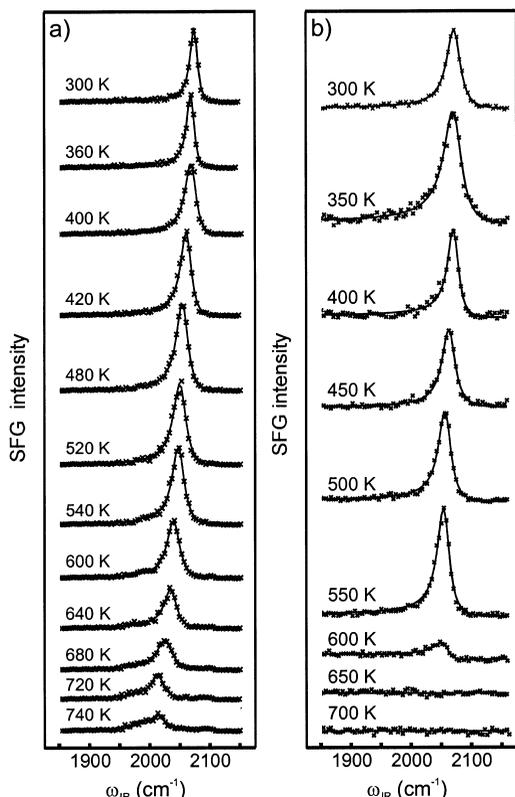


FIG. 5. (a) SFG spectra of CO terminally adsorbed on Rh(111) recorded at different substrate temperatures at a constant CO pressure of 1 mbar. The appearance of an additional low-frequency vibrational feature for substrate temperatures  $T_s \geq 600$  K marks the onset of a new non-reversible dissociative CO adsorption mechanism (for details, see text). (b) SFG spectra of CO terminally adsorbed on Rh(111) recorded during CO oxidation under laminar flow conditions at a total pressure of 20 mbar in a stagnation point flow (CO, 15 sccm; O<sub>2</sub>, 30 sccm; Ar, 105 sccm; flow velocity 2.5 cm/s). Experimental data points are represented by crosses, and the solid lines represent results of numerical simulations of the experimental spectral line shapes used to determine on-top CO stretching vibrational frequency  $\omega_{\text{CO}}$  [14]. In the CO oxidation measurements, Ar was employed as in inert buffer gas and as an internal standard for the mass spectrometric determination of the CO<sub>2</sub> production rate shown in Fig. 7b (for details, see Ref. [11]).

low-frequency side of the on-top CO vibrational band is already noticeable. Fig. 6c finally shows an “SFG spectrum,” recorded for  $T_s = 680$  K after the CO pressure was raised to 100 mbar, in which no vibrational resonant signal can be discerned anymore. Comparison of the postreactive AE spectrum (Fig. 6c) with the one of the clean Rh surface (Fig. 6a) demonstrates that considerable amounts of

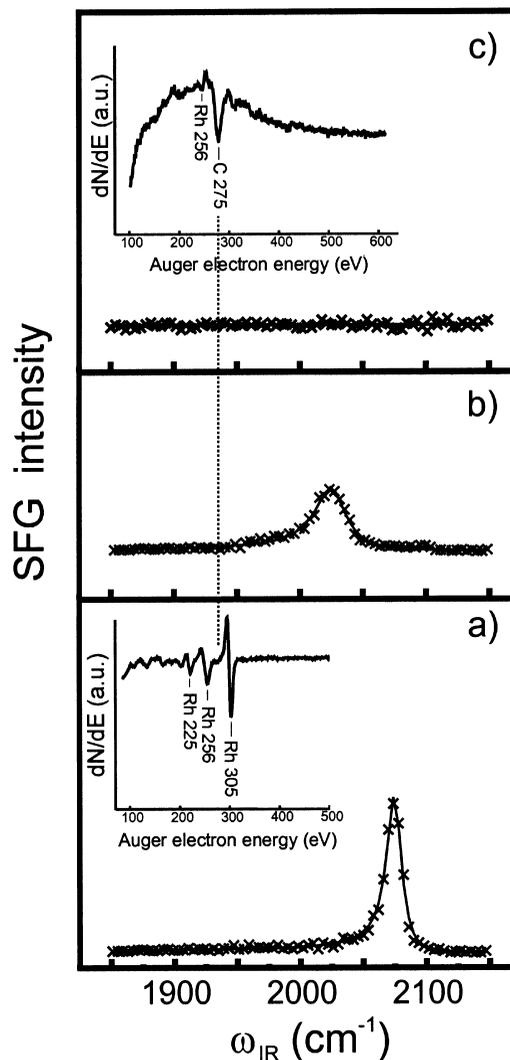


FIG. 6. (a) SFG spectrum of on-top adsorbed CO recorded at a CO pressure of 1 mbar and a substrate temperature of 300 K. The AE spectrum of the clean surface measured before the Rh substrate was exposed to CO is depicted as an insert. (b) SFG spectrum obtained after the substrate temperature was increased to  $T_s = 680$  K. (c) An “SFG spectrum,” recorded for  $T_s = 680$  K after the CO pressure was raised to 100 mbar, in which no vibrational resonant signal could be discerned anymore. The fact that also after reducing the substrate temperature no noticeable vibrational resonant signal in the SFG spectra reappeared confirmed the irreversibility of the CO adsorption process under these pressure and temperature conditions. The AE spectrum of the Rh surface measured after the substrate temperature was reduced to 300 K and after evacuation of the reaction chamber down to about  $10^{-9}$  mbar is depicted as an insert. Comparison of the latter postreactive AE spectrum with the one of the clean Rh surface shown in (a) demonstrates that considerable amounts of surface carbon, C(s), are deposited during the high-temperature and high-pressure adsorption of CO (for details, see text).

surface carbon, C(s), are deposited during “high-temperature” and “high-pressure” dissociative adsorption of CO. The fact that in contrast to most recent CO dissociation studies on Pt(111) [10], no oxygen signal was observed in the postreactive AE spectrum indicates that on Rh(111) the dissociation of CO proceeds predominately via the exothermic Boudouard reaction:  $2\text{CO} \rightarrow \text{C(s)} + \text{CO}_2$ . The downshift in the CO on-top stretching frequency observed in the present and in the previous [7] room-temperature CO adsorption studies for CO pressures  $\geq 100$  mbar (Fig. 3a) and the appearance of a new low-frequency vibrational feature for substrate temperatures  $T_s \geq 600$  K (see Fig. 5a) is due to the formation of on-top CO coadsorbed with carbon on the surface rather than due to a reversible adsorbate-induced surface roughening, as was tentatively proposed in Ref. [6].

### CO Oxidation

SFG spectra recorded during CO oxidation are depicted in Fig. 5b. The spectra were evaluated using the CO frequency versus CO coverage curve depicted in Fig. 4b to determine the total CO coverage as a function of substrate temperature, as depicted in Fig. 7a. The  $\text{CO}_2$  production rate simultaneously measured using mass spectrometry is reproduced in Fig. 7b. Postreactive AE spectra revealed that only trace amounts of surface carbon and Rh surface oxides are formed during CO oxidation under the present reagent pressure and substrate temperature conditions. The formation of Rh surface oxides, which results in an efficient deactivation of the catalyst surface, has been observed in previous CO oxidation studies on Rh(111) for oxygen partial pressures of about 500 mbar [16].

As can be seen in Fig. 7a, the presence of  $\text{O}_2$  in the stagnation flow does not result in a reduction of the CO surface coverage, indicating that adsorbed CO efficiently blocks the adsorption of oxygen up to a substrate temperature of about 400 K [16]. Only for temperatures above  $T_s = 400$  K does the CO coverage start to decrease from the saturation value of  $\theta_{\text{CO}} = 0.75$ . At the same time, the onset of  $\text{CO}_2$  production becomes noticeable, as indicated by the results shown in Fig. 7b. In the temperature range  $T_s = 400$ –600 K, the CO equilibrium coverage decreases linearly with substrate temperature. In this temperature range, the rate-determining step for  $\text{CO}_2$  production is the dissociative adsorption of  $\text{O}_2$ , which is hindered by the high CO surface coverage [16]. The sudden decrease in CO coverage at  $T_s > 600$  K in Fig. 7a is due to a transition from a predominately CO-covered surface state to an O-covered state originating from an increase of dissociative oxygen adsorption with decreasing CO coverage and the increase of the surface reaction rate.

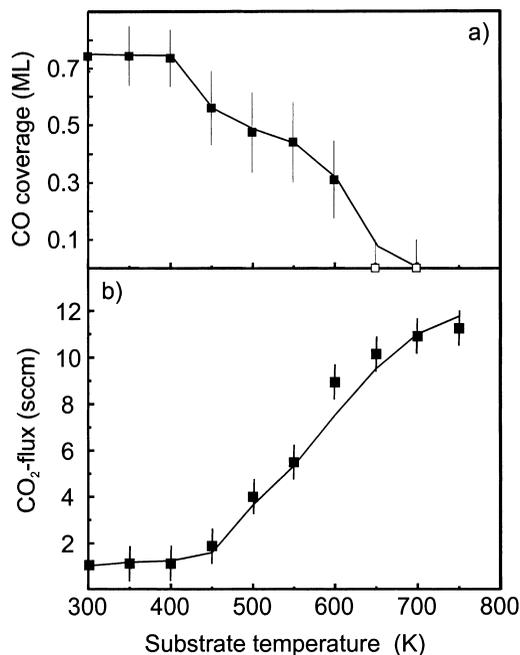


FIG. 7. (a) CO surface coverage (filled squares) as a function of the Rh(111) substrate temperature obtained during CO oxidation. (b)  $\text{CO}_2$  production rate simultaneously measured using mass spectrometry. Measurements were performed at a total pressure of 20 mbar under laminar flow conditions in a stagnation point flow ( $\text{CO}$ , 15 sccm;  $\text{O}_2$ , 30 sccm; Ar, 105 sccm; flow velocity 2.5 cm/s). The solid lines in (a) and (b) represent the results of a numerical simulation corresponding to the conditions of the experiment. Details of the surface reaction mechanism are given in the text and in Table 1.

The solid lines depicted in Fig. 7a and 7b represent the results of a numerical simulation based on the model of a reactive stagnation point flow directed toward a reactive surface [12]. The surface processes are described by a mean-field (MF) model [17]. The surface reaction mechanism employed is based on a Langmuir-Hinshelwood (LH) scheme for CO oxidation, which includes molecular adsorption and desorption of CO, dissociative adsorption of molecular oxygen, as well as the formation of  $\text{CO}_2$  through reaction of the adsorbed CO and O species (Table 1). In the surface reaction model, it was assumed that the oxygen sticking probability depends on the actual CO surface coverage, decreasing rapidly from an initial value of 0.9 in the limit of zero CO coverage [18,19] to about 1% of this value at  $\theta_{\text{CO}} = 0.3$ . The latter behavior of the oxygen sticking probability reflects the reduced availability of adjacent free adsorption sites for oxygen adsorption as a result of the repulsive interaction between the CO adsorbate molecules [16].

TABLE 1  
Surface reaction mechanism and kinetic parameters for the oxidation of CO on Rh(111)

Reaction	$\nu_0$ ( $s^{-1}$ )	$\nu_1$ ( $s^{-1}$ )	$E_0$ (kcal/mol)	$E_1$ (kcal/mol)	$S_0$	Ref.
O <sub>2</sub> adsorption					0.9	[18,19]
O <sub>2</sub> desorption	$3 \times 10^5$		24			[20]
CO adsorption					0.8	[21]
CO desorption	$1.33 \times 10^{14}$	$1.0 \times 10^{10}$	32.3	18.3		[21]
CO <sub>2</sub> production	$1 \times 10^{12}$		25.3			[16,22]

Note:  $\nu_0$  and  $\nu_1$  ( $E_0$  and  $E_1$ ) are the pre-exponential factors (activation energies) for an isolated molecule and for a molecule at saturation coverage, respectively.

### Conclusions

The present CO adsorption studies demonstrated reversible molecular adsorption of CO on Rh(111) up to a pressure of 10 mbar. For CO pressures above 10 mbar, the onset of a new irreversible dissociative CO adsorption mechanism on Rh(111) could be observed beginning at a substrate temperature of 300 K. At this temperature, as well in the substrate temperature range 600–800 K, CO dissociation was found to result in the formation of carbon on the surface as the only detectable dissociation product, indicating that CO dissociation on Rh(111) occurs via the Boudouard reaction:  $2CO \rightarrow C(s) + CO_2$ . The good agreement which could be obtained between the results of CO oxidation experiments and numerical simulations for CO and O<sub>2</sub> partial pressures as typically present in the exhaust gas of spark-ignited IC engines demonstrated that under these conditions, Rh(111)-catalyzed CO oxidation can be quantitatively described in the framework of a MF approach employing an LH surface reaction scheme which involves the reaction of adsorbed CO molecules with chemisorbed atomic oxygen species.

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### REFERENCES

- Ertl, G., Knözinger, H., and Weitkamp, J. (eds.), *Handbook of Heterogeneous Catalysis*, Vol. 4, VCH-Verlag, Weinheim, 1997.
- Somorjai, G. A., *Introduction to Surface Chemistry and Catalysis*, Wiley, New York, 1994.
- Heck, R. M., and Farrauto, R. J., *Catalytic Air Pollution Control*, Wiley, New York, 1995.
- Zhdanov, V. P., and Kasemo, B., *Surf. Sci. Rep.* 29:31 (1997) and references therein.
- Van Hove, M. A., *Isr. J. Chem.* 38:349 (1998).
- Somorjai, G. A., and Rupprechter, G., *J. Phys. Chem. B* 103:1623 (1999).
- Somorjai, G. A., Su, X., McCrea, K. R., and Rider, K. B., *Top. Catal.* 8:23 (1999).
- Cernota, P., Rider, K., Yoon, H. A., Salmeron, M., and Somorjai, G. A., *Surf. Sci.* 445:249 (2000).
- Kung, K. Y., Chen, P., Wei, F., Shen, Y. R., and Somorjai, G. A., *Surf. Sci.* 463:627 (2000).
- Volpp, H.-R., and Wolfrum, J., in *Applied Combustion Diagnostic* (K. Kohse-Höinghaus and J. Jeffries, eds.), Taylor & Francis, New York, 2002.
- Härle, H., Lehnert, A., Metka, U., Volpp, H.-R., Willms, L., and Wolfrum, J., *Appl. Phys. B.* 68:567 (1999).
- Kissel-Osterrieder, R., Behrendt, F., Warnatz, J., Metka, U., Volpp, H.-R., and Wolfrum, J., *Proc. Combust. Inst.* 28:1341 (2000).
- Shen, Y. R., *Nature* 337:519 (1989) and references therein.
- Härle, H., Metka, U., Volpp, H.-R., and Wolfrum, J., *Phys. Chem. Chem. Phys.* 1:5059 (1999) and references therein.
- Bandara, A., Dobashi, S., Kubota, J., Onda, K., Wada, A., Domen, K., Hirose, C., and Kano, S. S., *Surf. Sci.* 387:312 (1997).
- Peden, C. H. F., Goodman, D. W., Blair, D. S., Berlowitz, P. J., Fisher, G. B., and Oh, S. H., *J. Phys. Chem.* 92:1563 (1988).
- Deutschmann, O., Behrendt, F., and Warnatz, J., *Catal. Today* 46:155 (1998).
- Van Hove, M. A., Weinberg, W. H., and Chan, C.-M., *Low-Energy Electron Diffraction*, Springer-Verlag, Berlin, 1986.
- Yates Jr., J. T., Thiel, P. A., and Weinberg, W. H., *Surf. Sci.* 82:45 (1979).
- Root, T. W., Schmidt, L. D., and Fisher, G. B., *Surf. Sci.* 134:30 (1983).
- Seebauer, E. G., Kong, A. C. F., and Schmidt, L. D., *Appl. Surf. Sci.* 31:163 (1988).
- Hopstaken, M. J. P., and Niemantsverdriet, J. W., *J. Chem. Phys.* 113:5457 (2000).

## COMMENTS

*Ian Reid, BP Chemicals, UK.* Given the carbon formation mechanism on Rh catalyst, are you able to comment on whether this process also occurs on platinum? Additionally can you comment on the temperature limit to maintain the catalyst with a low carbon average for Pt compared to Rh?

*Author's Reply.* Employing IR-VIS SFG along with post-reactive AES studies, it could be demonstrated that, contrary to the general believe of surface science that CO cannot dissociate on platinum, CO does indeed dissociate on a Pt(111) single-crystal catalyst [1,2]. The major difference between the CO/Rh(111) and CO/Pt(111) adsorption system, however, is that for the CO/Rh(111) system, dissociative adsorption of CO occurs—as has been shown in the

present contribution—already at room temperature, while in case of CO/Pt(111) dissociation and hence surface carbon formation starts only at a catalyst temperature above ca. 500 K at a CO pressure of 1 mbar [3].

## REFERENCES

1. Kung, K. Y., Chen, P., Wei, F., Shen, Y. R., and Somorjai, G. A., *Surf. Sci.* 463:627 (2000).
2. Volpp, H.-R., and Wolfrum, J., *Applied Combustion Diagnostic* (K. Kohse-Höinghaus and J. Jeffries, eds.), Taylor & Francis, New York, 2002.
3. Metka, U., Schweitzer, M. G., Volpp, H.-R., and Wolfrum, J., unpublished data.